A PENALIZATION METHOD TO HANDLE THE INTERFACE BETWEEN A FREE-FLUID REGION AND A FIBROUS POROUS MEDIUM

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The coupling between the flow through a fibrous porous medium and that in a free-fluid region is studied. The flow dynamics inside the porous medium is described using the volume averaging method applied to the incompressible Navier-Stokes equations in the laminar regime. The two different flow domains are coupled via a penalization method that consists in varying the porous medium properties (porosity and permeability) continuously across the interface. This approach permits the use of the same set of the equations throughout the whole domain. The averaging method is validated against simulations which fully account for the presence of cylindrical fibers positioned at the bottom wall of a square driven cavity. Numerical experiments are carried out for two different Reynolds numbers, large enough to ensure that inertial effects inside the porous domain are not negligible. Good agreement is found when comparing the two approaches.

1. INTRODUCTION

The problem of a fluid flowing above and through porous media is prototypical of many natural flow systems. Several animals present some sort of porous coatings, the most well-known examples being perhaps the denticles of sharks (Dean and Bhushan, 2010) and the feathers of birds (Lilley, 1998). Some of these flows display rich interactions between the porous medium and the exterior flow field, for example in the form of vortex structures near the dividing surface (Jimenez et al., 2001). These vortices can modify the energy spectrum of the flow field (Finnigan, 2000), suggesting the use of porous layers as synthetic, passive control devices to delay separation and/or reduce drag (Klausmann and Ruck, 2017; Mimeau et al., 2017; Zampogna et al., 2018).

Although the set of equations for the flow both inside and outside the porous medium is well established, the problem of the interface condition between a porous medium and a free fluid is still open. Ehrhardt (2012) has given a concise but very clear introduction to the coupling problem; recent advances are reported by Angot et al. (2017), Lācis and Bagheri (2017) and Zampogna et al. (2018).

Approaches used to handle the interface can be classified into two groups: the *one-domain-approach* (ODA) and the *two-domain-approach* (TDA). In the TDA the whole domain is split into two and boundary conditions at the interface have to be specified. Historically, the necessity of such a treatment was mainly due to the difference of order Stokes equations and the Darcy ones, that renders them incompatible at the interface. The Brinkmann model "adjusts" the order of the porous medium equations so that continuity of velocity and traction vectors can be enforced; however, the validity of the viscous correction to the Darcy law inside the porous medium has been questioned (Nield, 1991). The TDA was followed by Beavers and Joseph (1967), Mikelić and Jäger (2000), Ochoa-Tapia and Whitaker (1995)

and Le Bars and Worster (2006). These works have in common the fact that a certain slip velocity has to be specified at the interface. For example, the Beavers and Joseph (1967) condition to leading order reads:

$$u_\beta(x, \Gamma^+) = \frac{\sqrt{K_{11}}}{\alpha} \frac{\partial u_\beta(x, \Gamma^+)}{\partial y},$$

where u_β is the velocity vector tangential to the dividing surface, whose normal direction is y. Γ^+ represents the wall normal coordinate right above the interface, K_{11} is the permeability component in the tangential direction and α is a coefficient based on the porous medium structure and geometry. Other formulations change and/or extend this equation, basically maintaining a slip velocity at the interface, function of one or more parameters which can be tuned to fit experimental data.

On the contrary, in the ODA approach the final averaged equations are valid through the whole domain and the quantities that define the presence of the porous media, i.e. the porosity and the inverse of the permeability, vanish in the free fluid region. This method is also known as *penalization method*. One of the first applications of the penalization method was described by Caltagirone (1994). Later on, it was used by many other authors, including Bruneau and Mortazavi (2004, 2008), Bruneau et al. (2010) and Hussong et al. (2011). The two approaches (TDA and ODA) require at least one parameter to close the formulation. The advantage of using the penalization method is that the parameter needed is the spatial distribution of the porosity field which is easily available on a known medium geometry. However, it is still not clear how the permeability in the transition/interface zone should be varied. Most authors propose a sharp jump from the value in the porous medium to that in the free-fluid region. Neglecting the variation of permeability across the transition zone appears to be acceptable, even though examples of linear variation of this term exist (Caltagirone (1994)). Hussong et al. (2011) make a direct comparison with a DNS simulation which includes a discretization of all the pores and indicate that the variation of permeability is very important in order to have accurate comparison with high fidelity computations.

A direct comparison between the ODA and the TDA is presented by Cimolin and Discacciati (2013), who conclude that the macroscopic description of the interface provided by the two different methods is similar. They also point out that the penalization method has the advantage of being easily implemented in a Navier-Stokes solver without convergence problems, unlike the TDA.

There is evidence in the literature (Ochoa-Tapia et al. (2017)) that a transition zone the size of the pore scale exists, in which velocity and pressure exhibit a continuous variation rather than a steep one. It has been demonstrated by the same authors that the transition zone is physical and not a result of the averaging procedure.

The present work adopts the penalization approach with the porosity variation computed directly from the geometry of the fibrous medium via a moving average. The effective permeability is varied linearly at the interface with the same law as the porosity. This interface approach coupled with the macroscopic volume-averaged equations is validated against a full microscopic direct numerical simulation. Computations are performed on a closed cavity configuration with a lower porous layer. This represents a more difficult test bed for the porous/fluid coupling than the classical Poiseuille flow, because of the presence of recirculating motion, with both velocity components different from zero at the dividing surface.

2. CLOSED CAVITY PROBLEM DESCRIPTION

The configuration chosen to test our approach is the square cavity of side L, depicted in figure 1. The lateral and bottom walls are fixed and a constant velocity U_{top} is specified at the top side. On the front and back sides (i.e. along x_3) periodic boundary conditions are enforced. The distance between the front and the back side of the cavity is indicated as ℓ. A rigid porous medium made by regularly arranged fibers is set at the bottom of the cavity, of vertical extension equal to $h = L/3$. The *representative elementary volume*, REV, of the porous medium is a cubic cell of size ℓ^3 with a cylinder of diameter d at its center. The cylinders are disposed in a regular arrangement and 50 fibers are assumed to be present in the cavity (i.e. $\ell = 0.02 L$). The origin of the coordinate system is taken at the bottom left corner of the cavity.
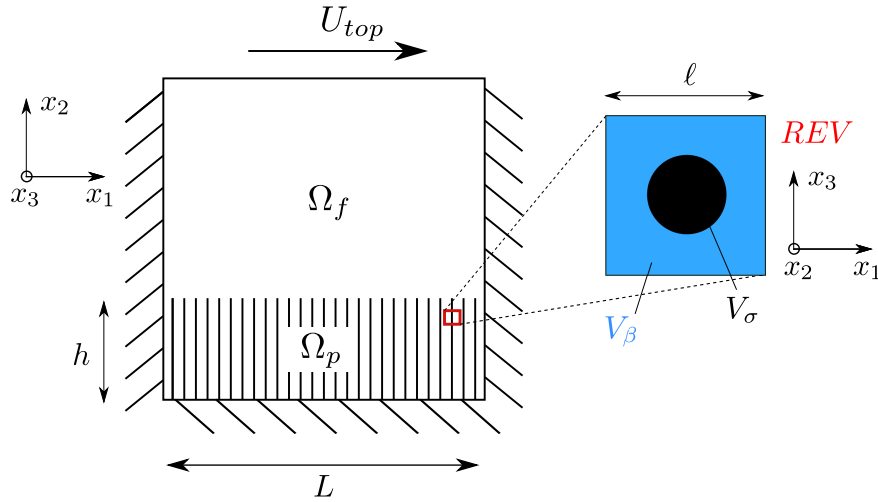
FIG. 1: Schematic of the closed cavity problem. The porous medium internal structure is depicted in the zoom which shows the REV geometry.

We denote by V_β the volume of the fluid phase within the REV, and by V_σ that of the solid phase, so that the porosity of the medium within the Ω_p region (cf. figure 1) is $\varepsilon = \dfrac{V_\beta}{V_\beta + V_\sigma} = 1 - \pi \left(\dfrac{d}{2\ell} \right)^2 = 0.8$. The macroscopic Reynolds number is $Re = \dfrac{U_{top} L}{\nu_\beta}$; it is taken sufficiently large for inertial effects within the porous medium to have some significance, at least in a layer below the interface. We remark that if inertial terms must be accounted for with a Darcy-like model, the permeability of the porous medium must be replaced by an *apparent* permeability which depends on both the amplitude and the orientation of the pore velocity (Luminari et al., 2018).

3. MICROSCOPIC APPROACH: DIRECT NUMERICAL SIMULATIONS

The most rigorous way to solve the problem above is to perform a full direct numerical simulation (DNS) in which the fluid flow around each fiber is well resolved. In this approach the incompressible Navier-Stokes equations are solved in three dimensions. The problem is however only weakly three dimensional, since a single REV along the x_3 axis is included, together with periodic boundary conditions. To complete the set of boundary conditions, no-slip is enforced at all the cavity walls, with the top wall moving at a prescribed speed. The mesh is fine enough to resolve the flow within the fibers and the spatial and time convergence is also ensured (Zampogna and Bottaro, 2016). The above setup is described by the set of equations:

$$\begin{cases} \dfrac{\partial \mathbf{v}_\beta}{\partial t} + \mathbf{v}_\beta \cdot \nabla \mathbf{v}_\beta = -\dfrac{1}{\rho_\beta} \nabla p_\beta + \nu_\beta \nabla^2 \mathbf{v}_\beta, \\ \nabla \cdot \mathbf{v}_\beta = 0, \\ \mathbf{v}_\beta = 0, \qquad \text{on} \quad x_1 = 0, L, \quad x_2 = 0, \\ \mathbf{v}_\beta = U_{top}, \qquad \text{on} \quad x_2 = L, \\ \mathbf{v}_\beta|_{x_3=0} = \mathbf{v}_\beta|_{x_3=\ell}, \\ p_\beta|_{x_3=0} = p_\beta|_{x_3=\ell}, \end{cases} \qquad (1)$$

where $\mathbf{v}_\beta$, p_β, ρ_β and ν_β stand, respectively, for velocity, pressure, density and kinematic viscosity of the fluid.

Once system (1) is solved, the microscopic fields (velocity and pressure) inside the porous medium are averaged

in order to get the homogenized macroscopic fields, $\langle \mathbf{v}_\beta \rangle^\beta$ and $\langle p_\beta \rangle^\beta$. The intrinsic averaging operator (Whitaker, 2013) is defined by:

$$\langle \psi_\beta \rangle^\beta = \frac{1}{V_\beta} \int_{V_\beta} \psi_\beta(\mathbf{x}) dV_\beta. \tag{2}$$

Such an operator is applied through the whole porous domain using a REV of dimension ℓ^3. The centroid of the REV, over which the averaging operation is performed, spans all the porous domain extension. An example of REV adopted in this case is depicted in figure 1, on the right. The choice of the REV size is trivial for ordered porous media, as in our case, however some technical aspects on the REV choice when the medium is disordered must be faced (Davit and Quintard, 2017). As a rule of thumb, the REV is the smallest fluid domain over which periodic boundary conditions can be applied. It should be noted that the averaging procedure yields a two dimensional averaged field as a result, the only non-zero values are in the x_1 and x_2 directions. This is due to the symmetry of velocity and pressure in the x_3 direction that returns zero averaged field.

4. MACROSCOPIC APPROACH: VOLUME-AVERAGED NAVIER-STOKES (VANS) METHOD

4.1 A brief description of the method

A more computationally convenient way to solve the problem is to apply the VANS method to derive a homogenized model for the flow inside the porous medium, described as a continuum.

In order to derive the averaged version of system (1) we first define the fundamental ingredients needed in the development. The first one is the intrinsic average operator (2), already introduced above. The second is the decomposition of any flow variable ψ into an intrinsic average part $\langle \psi \rangle^\beta$ plus a perturbation $\tilde{\psi}$, as:

$$\psi = \langle \psi \rangle^\beta + \tilde{\psi}.$$

Applying the above decomposition and the intrinsic average operator to the first two equations of system (1), and following Whitaker (1996), we have:

$$\frac{\partial \langle \mathbf{v}_\beta \rangle^\beta}{\partial t} + \frac{1}{\varepsilon} \nabla \cdot \left(\varepsilon \langle \mathbf{v}_\beta \rangle^\beta \langle \mathbf{v}_\beta \rangle^\beta \right) = -\frac{1}{\rho_\beta} \nabla \langle p_\beta \rangle^\beta + \nu_\beta \nabla^2 \langle \mathbf{v}_\beta \rangle^\beta + \frac{\nu_\beta}{\varepsilon} \nabla \varepsilon \cdot \nabla \langle \mathbf{v}_\beta \rangle^\beta +$$

$$+ \frac{\nu_\beta}{\varepsilon} \langle \mathbf{v}_\beta \rangle^\beta \nabla^2 \varepsilon + \frac{1}{V_\beta} \int_{A_{\beta\sigma}} \left(-\frac{\tilde{p}_\beta}{\rho_\beta} \mathbf{I} + \nu_\beta \nabla \tilde{\mathbf{v}}_\beta \right) \cdot \mathbf{n}_{\beta\sigma} dA, \tag{3}$$

$$\nabla \cdot \left(\varepsilon \langle \mathbf{v}_\beta \rangle^\beta \right) = 0, \tag{4}$$

upon neglecting in equation (3) the sub-REV-scale dispersion term (linked to $\langle \tilde{\mathbf{v}}_\beta \tilde{\mathbf{v}}_\beta \rangle^\beta$) which is often small in porous media flows (Breugem, 2005).

The surface integral term in equation (3) represents the drag (per unit mass) due to surface forces at the fluid-solid interface of the medium. It is called the Darcy-Forchheimer microscale force, $\mathbf{F}^m$. The equations are, however, often to be solved at the macroscale, so that a macroscale force model, $\mathbf{F}^M$, must be used to replace $\mathbf{F}^m$ in the governing equation. Such a model is based on a permeability tensor, $\mathbf{K}$, and a Forchheimer tensor, $\mathbf{F}$, and reads:

$$\mathbf{F}^M = -\nu_\beta \mathbf{K}^{-1}(\mathbf{I} + \mathbf{F}) \langle \mathbf{v}_\beta \rangle^\beta = -\nu_\beta \mathbf{H}^{-1} \langle \mathbf{v}_\beta \rangle^\beta,$$

where $\mathbf{H} = \mathbf{K}^{-1}(\mathbf{I} + \mathbf{F})$ is called the *apparent* permeability tensor. The system is closed by imposing $\mathbf{F}^m = \mathbf{F}^M$. One of the main aspects of the VANS approach consists in the identification of the permeability and Forchheimer tensors. Some empirical regressions are available in the literature for simple porous media geometries (Carman, 1937; Kozeny, 1927) in the limit of Stokes flow within the pores. It is however also possible to derive some generalized closure problems for the solution of the two tensors, as discussed by Whitaker (1986, 1996).

Finally, the complete set of VANS equation reads:

$$
\begin{cases}
\dfrac{\partial \langle \mathbf{v}_\beta \rangle^\beta}{\partial t} + \dfrac{1}{\varepsilon} \nabla \cdot \left[\varepsilon \langle \mathbf{v}_\beta \rangle^\beta \langle \mathbf{v}_\beta \rangle^\beta \right] = -\dfrac{1}{\rho_\beta} \nabla \langle p_\beta \rangle^\beta + \nu_\beta \nabla^2 \langle \mathbf{v}_\beta \rangle^\beta, \\
\qquad\qquad\qquad - \nu_\beta \varepsilon \mathbf{H}^{-1} \langle \mathbf{v}_\beta \rangle^\beta + \dfrac{\nu_\beta}{\varepsilon} \nabla \varepsilon \cdot \nabla \langle \mathbf{v}_\beta \rangle^\beta + \dfrac{\nu_\beta}{\varepsilon} \langle \mathbf{v}_\beta \rangle^\beta \nabla^2 \varepsilon, \\
\nabla \cdot \left(\varepsilon \langle \mathbf{v}_\beta \rangle^\beta \right) = 0, \\
\langle \mathbf{v}_\beta \rangle^\beta = 0 \qquad \text{at} \quad x_1 = 0, L \quad x_2 = 0, \\
\langle \mathbf{v}_\beta \rangle^\beta = U_{top} \qquad \text{at} \quad x_2 = L.
\end{cases}
\tag{5}
$$

The boundary conditions are the same as the DNS approach except for the x_3 dimension that in the present case disappears through averaging. The solution of system (5) gives directly the averaged velocity and pressure fields to be compared to the averaged DNS fields.

4.1.1 Interface treatment

In order to use the so-called penalization method, the porosity field and the effective permeability have to be defined in the whole domain, i.e. Ω_p and Ω_f. In the free fluid the porosity is, of course, unitary and the effective permeability infinite. With such numerical values the Navier-Stokes system (1) is retrieved from system (5) after some simplifications. In the porous medium far from the interface the porosity is constant and set equal to 0.8. The permeability is also constant and the two independent components of the tensor have been taken from *a posteriori* evaluations of the homogenized-DNS problem. This requires the inversion of the Darcy system $\langle \mathbf{v}_\beta \rangle^\beta = -\dfrac{\mathbf{H}}{\varepsilon \mu_\beta} \nabla \langle p_\beta \rangle^\beta$. The numerical values for $\mathbf{H}$, given in table 1, are different at the macroscopic Reynolds numbers of 100 and 1000, an indication of the fact that inertia through the pores is no more negligible. The values in table 1 are by no mean exact: they represent the peak values of the computed distributions. The apparent permeability tensor $\mathbf{H}$ is diagonal; this is consistent with the results of Luminari et al. (2018) for low pore Reynolds number. It turns out that in the cavity the pore Reynolds number, based on the local velocity and the diameter of the fibers, is always below 5 for the cases tested.

The most delicate part is the matching of properties across the dividing surface. The exact profile for the porosity field can be computed knowing the geometry of the medium. By a moving average procedure it is easily found that ε is equal to:

$$
\varepsilon(x_2) = \begin{cases}
1 & x_2 \geqslant (h + \ell/2), \\
\varepsilon + \dfrac{1 - \varepsilon}{\ell} \left[x_2 - (h - \ell/2) \right] & (h - \ell/2) < x_2 < (h + \ell/2), \\
\varepsilon & x_2 \leqslant (h - \ell/2),
\end{cases}
\tag{6}
$$

to within the averaging approximation. A similar relation is used for the inverse of the effective permeability field, with H_{ii} referring to the effective permeability components of the deep medium, reported in table 1.

$$
H_{ii}^{-1}(x_2) = \begin{cases}
0 & x_2 \geqslant (h + \ell/2), \\
H_{ii}^{-1} - \dfrac{H_{ii}^{-1}}{\ell} \left[x_2 - (h - \ell/2) \right] & (h - \ell/2) < x_2 < (h + \ell/2), \\
H_{ii}^{-1} & x_2 \leqslant (h - \ell/2).
\end{cases}
\tag{7}
$$

Re	$H_{11} = H_{22}$	H_{33}
100	$2.63 \cdot 10^{-2}$	$5.49 \cdot 10^{-2}$
1000	$2.65 \cdot 10^{-2}$	$5.63 \cdot 10^{-2}$

TABLE 1: Apparent permeability values from Zampogna and Bottaro (2016).

Re	e_u	e_v	$e_{p_{x_1}}$	$e_{p_{x_2}}$
100	$2.18 \cdot 10^{-9}$	$2.12 \cdot 10^{-9}$	$3.38 \cdot 10^{-3}$	$7.36 \cdot 10^{-5}$
1000	$3.95 \cdot 10^{-8}$	$7.01 \cdot 10^{-8}$	$1.06 \cdot 10^{-3}$	$4.78 \cdot 10^{-6}$

TABLE 2: Relative $||L_2||$ error between the VANS and the DNS approaches at the interface, for the two different Reynolds numbers.

The data analysis by Luminari et al. (2018) suggests that the components of **H** are mostly driven by the porosity, so it is acceptable to assume that the same dependence on x_2 occurs for both the porosity and the permeability fields. The analysis in Kozeny (1927) and Ergun and Orning (1949) also shows that, in other porous media geometries, the permeability follows a linear trend on the porosity. For comparison purposes, we have also tested a step variation of the permeability at the dividing surfaces (results not shown), finding large differences when compared to the direct simulation results. Finally, observe also that in equation (5) the terms containing the first derivative of the porosity remain as sources in the equations near the interface, whereas the laplacian of ε disappears.

5. CAVITY FLOW AT $RE = 100$

This section presents the comparison between the microscopic and macroscopic approaches for the cavity at $Re = 100$. The two different sets of equations are solved using the finite volume method implemented in the OpenFOAM library (Weller et al., 1998). In the case of the VANS approach a specific solver has been developed to account for all the extra terms present in system (5) as compared to the Navier-Stokes equations. Figures 2 to 3 show the pressure gradient terms and the velocity fields for the two different approaches.

Each field is made non-dimensional using the macroscopic length L and the velocity scale, U_{top}, as follows:

$$u^* = u/U_{top}, \qquad v^* = v/U_{top},$$
$$\frac{\partial p^*}{\partial x_1{}^*} = \frac{L}{\rho_\beta U_{top}^2} \frac{\partial p}{\partial x_1}, \qquad \frac{\partial p^*}{\partial x_2{}^*} = \frac{L}{\rho_\beta U_{top}^2} \frac{\partial p}{\partial x_2}.$$

At Reynolds number equal to 100 a good agreement is found for both the velocity components and the pressure gradient (figure 2). The contours and the location of the local minima and maxima are the same for the two approaches. Focusing on the numerical values, for some fields the relative errors are not negligible; however, the trends are always well captured by the volume-averaged approach, and the streamlines inside the porous domain are in very good agreement with the DNS data. The horizontal pressure gradient at the interface (fig. 4) is quite over-estimated by the VANS approach whereas the vertical component shows a relatively good agreement. Some differences between the two models have to be expected since in the VANS approach the micro-scale flow behavior is modeled. This means that some of the small scale structures that the DNS is able to retain, are lost in the macroscopic approach. However, figure 3 shows that the two approaches produce very similar velocities profile both near the interface and within the domains Ω_p and Ω_f.

To quantify the error between the two approaches right at the interface, $x_{2\,itf}^* = 0.33$, we define a metric as:

$$e_q = \int_0^1 \left(q_{DNS}(x_1^*, x_{2\,itf}^*) - q_{VANS}(x_1^*, x_{2\,itf}^*) \right)^2 d\,x_1^*, \tag{8}$$

with q equal to u^*, v^*, $\dfrac{\partial p^*}{\partial x_1{}^*}$ and $\dfrac{\partial p^*}{\partial x_2{}^*}$. The values from table 2 confirm that the errors associated with the two velocity components are very low; on the contrary for the pressure gradient the horizontal component displays a non-negligible variation. These small discrepancies are probably the price to pay for having neglected the terms linked to $\langle \tilde{\mathbf{v}}_\beta \tilde{\mathbf{v}}_\beta \rangle^\beta$ in equation (3), and for the approximation made at the interface for $\mathbf{H}^{-1}$. The advantages of using the VANS equations in terms of computer time and storage are however so high that we believe that our effort is worthwhile.

6. CAVITY FLOW AT $RE = 1000$

The same comparison has also been carried out for a Reynolds number equal to 1000 and the results within the porous medium are shown in figures 5 to 8. For this case similar conclusions as in the previous case can be made. Both the velocity and the pressure fields display good agreement between the "exact" (DNS) solution and that obtained with the VANS system, both within the porous layer (figure 5) and the free-fluid domain (not shown). The velocity at the dividing surface ($x_2{}^* = 0.33$) is very well described by the volume-averaged resolution of the equations (figure 6), as well as the vertical pressure gradient. The $\dfrac{\partial p^*}{\partial x_1{}^*}$ term shows the same trend, but the VANS system enhances the value of the gradient, albeit less then in the lower Re case. This is also borne by the measure reported in table 2. The vertical velocity distribution through the domain at $x_1{}^* = 0.5$ is in excellent agreement between the two approaches (figure 7), and in particular the zooms around the interface demonstrate that the VANS approach is reliable; such plots should be compared to those by Zampogna and Bottaro (2016) from the same configuration, to appreciate even more the accuracy of the volume averaged equation in the form of system (3), (4), as well as the simple choice made for the variation of porosity and permeability across the dividing surface.

Focusing on the zone around the porous interface in figure 8, the minor differences between the DNS and homogenized approach are clear. The DNS shows oscillations in both the vertical and horizontal velocity components due to the presence of the fibers; on the contrary, in the homogenized approach these local oscillations are smoothed out by the averaging operation. However, the oscillations have a very small amplitude and to make them visible the range of values plotted needs to be suitably chosen (see the velocity scales on the right of figure 8).
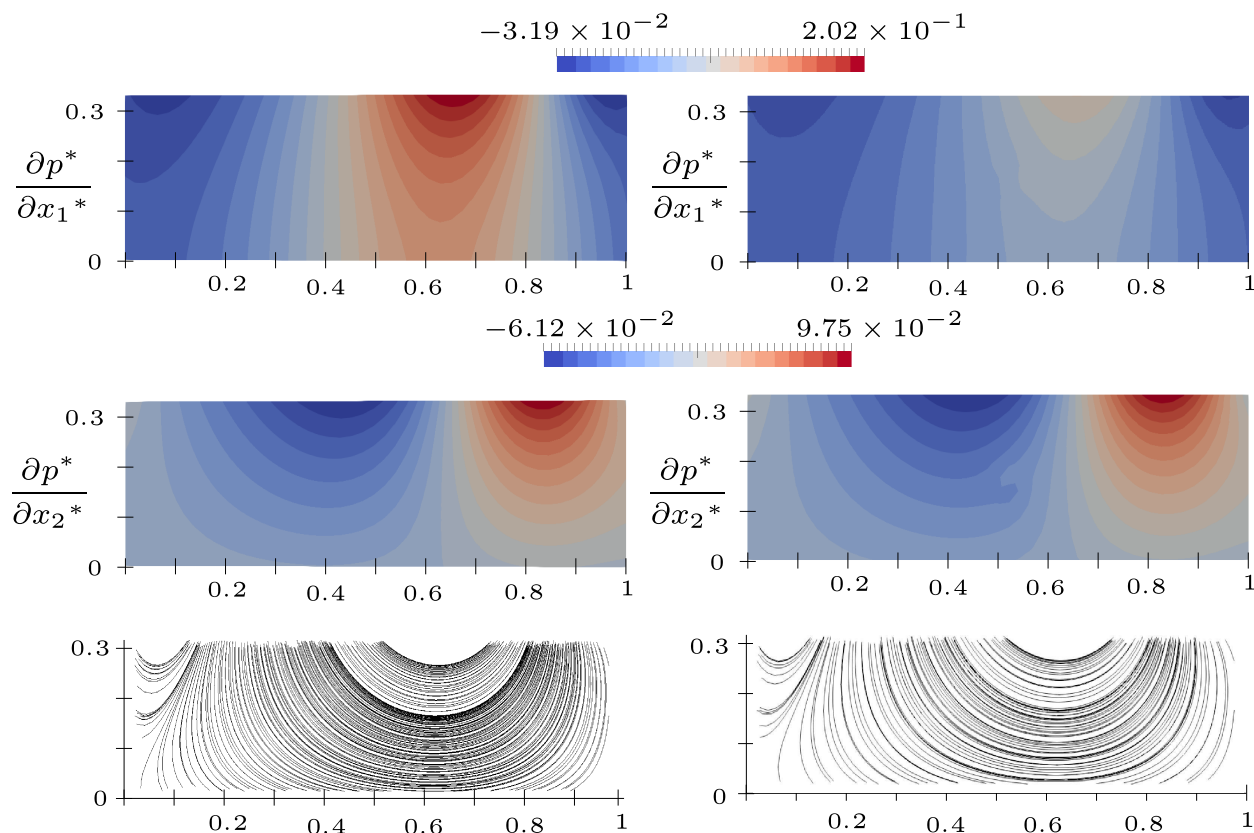

FIG. 2: Left: VANS approach. Right: Homogenized DNS approach. The figures show, from top to bottom, the two components of the pressure gradient and the streamlines inside the porous domain Ω_p for $Re = 100$.
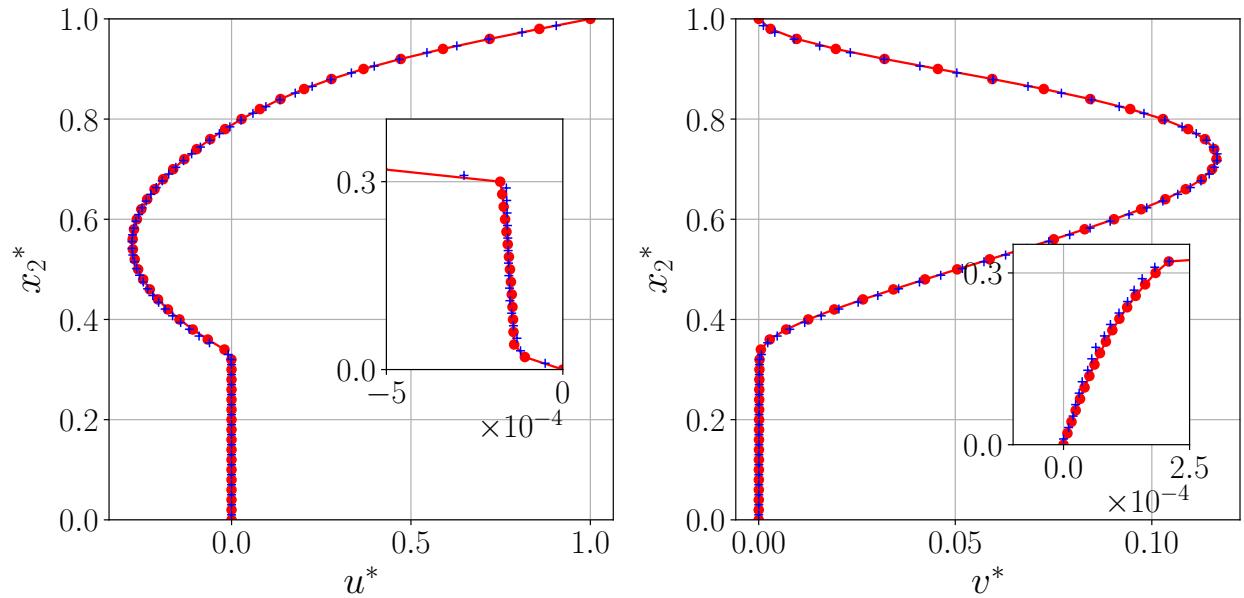
FIG. 3: View of the macroscopic profile of u^* (left frame) and v^* (right frames) for $x_1^* = 0.5$ (middle of the cavity) for the VANS (red line with circles) and the DNS approaches (blue line with crosses) at $Re = 100$.

7. CONCLUSIONS

The VANS approach has been used to study the flow field inside a cavity that presents a porous medium at its bottom. A formulation of the penalization method has been proposed for the interface treatment; it is based on the observation that for fibrous media the porosity profile at the interface between the porous region and the free-fluid domain can be simply computed by a moving average. Knowing the porosity profile we impose the same behavior also for the apparent permeability, since results in Luminari et al. (2018) show the strong link between these two quantities even for varying velocity amplitude and flow angles. This approach simplifies the coupling between the two domains, Ω_f and Ω_p, allowing to use the same set of equations throughout. Both ODA and TDA need at least one free parameter, for DNS or experimental data to be properly fit. In our case, this degree of freedom is represented by the choice of a linear trend for the components of the apparent permeability.

The proposed approach has been tested in a configuration in which both vertical and horizontal momentum transfer are present. We have also explored two Reynolds number for which inertial effect inside the porous medium are not negligible. The two test simulations conducted display promising results. The error metrics are reasonably low for all the measured quantities, with the possible exception of the horizontal pressure gradient which shows differences in the magnitude, but not in the peak positions. Such small differences might also be ascribed to our treatment of the sub-REV-scale dispersion terms. Despite them, we believe that the evidence provided is sufficiently convincing in favor of the averaging approach, which is capable to reproduce the rich dynamics inside porous media at a fraction of the computational cost of a complete DNS.
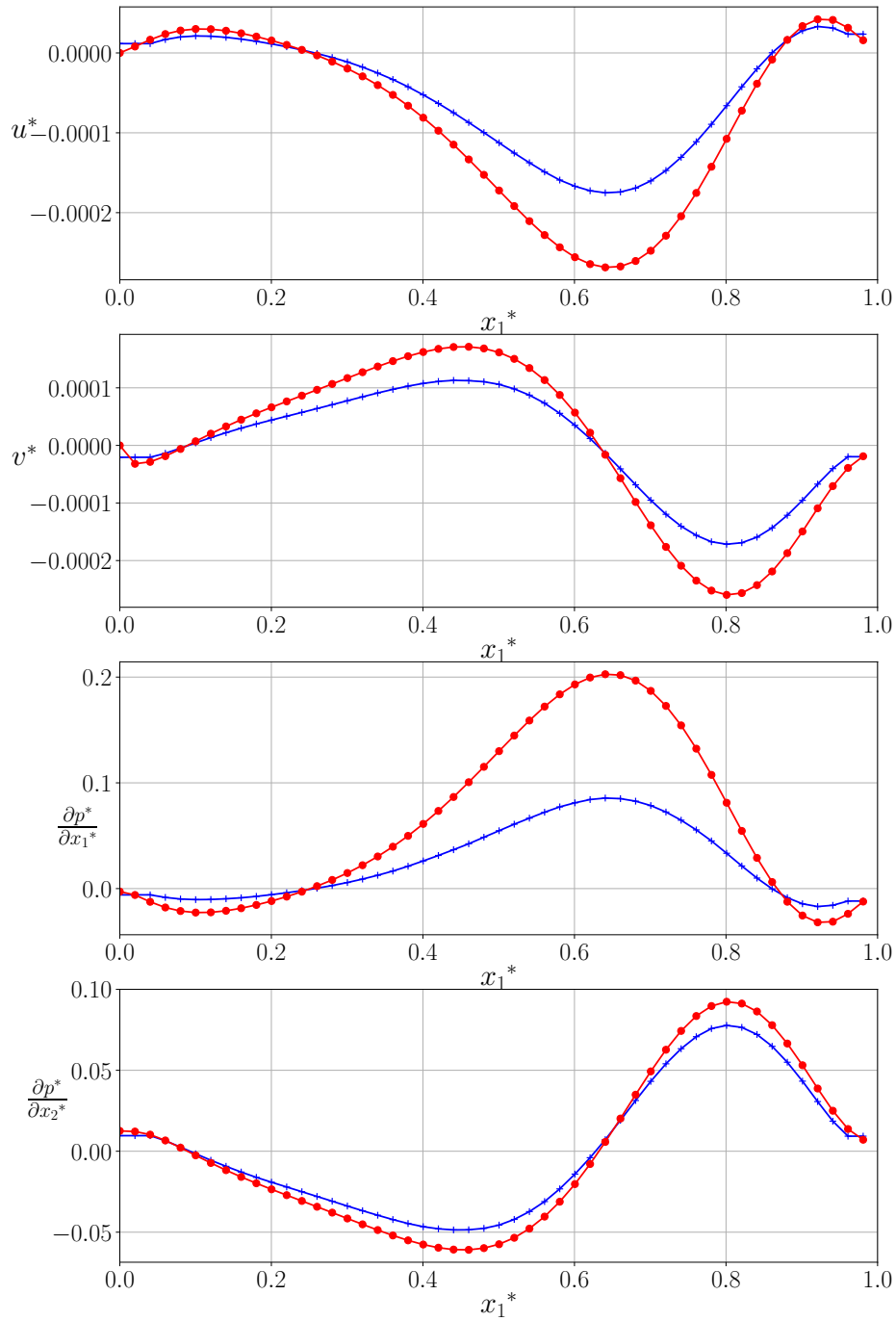
ACKNOWLEDGMENTS

FIG. 4: View of the macroscopic profile of u^*, v^*, $\dfrac{\partial p^*}{\partial x_1^*}$ and $\dfrac{\partial p^*}{\partial x_2^*}$, for $x_2^* = 0.33$ (interface position) for the VANS (red lines with circles) and the DNS approaches (blue lines with crosses) at $Re = 100$.

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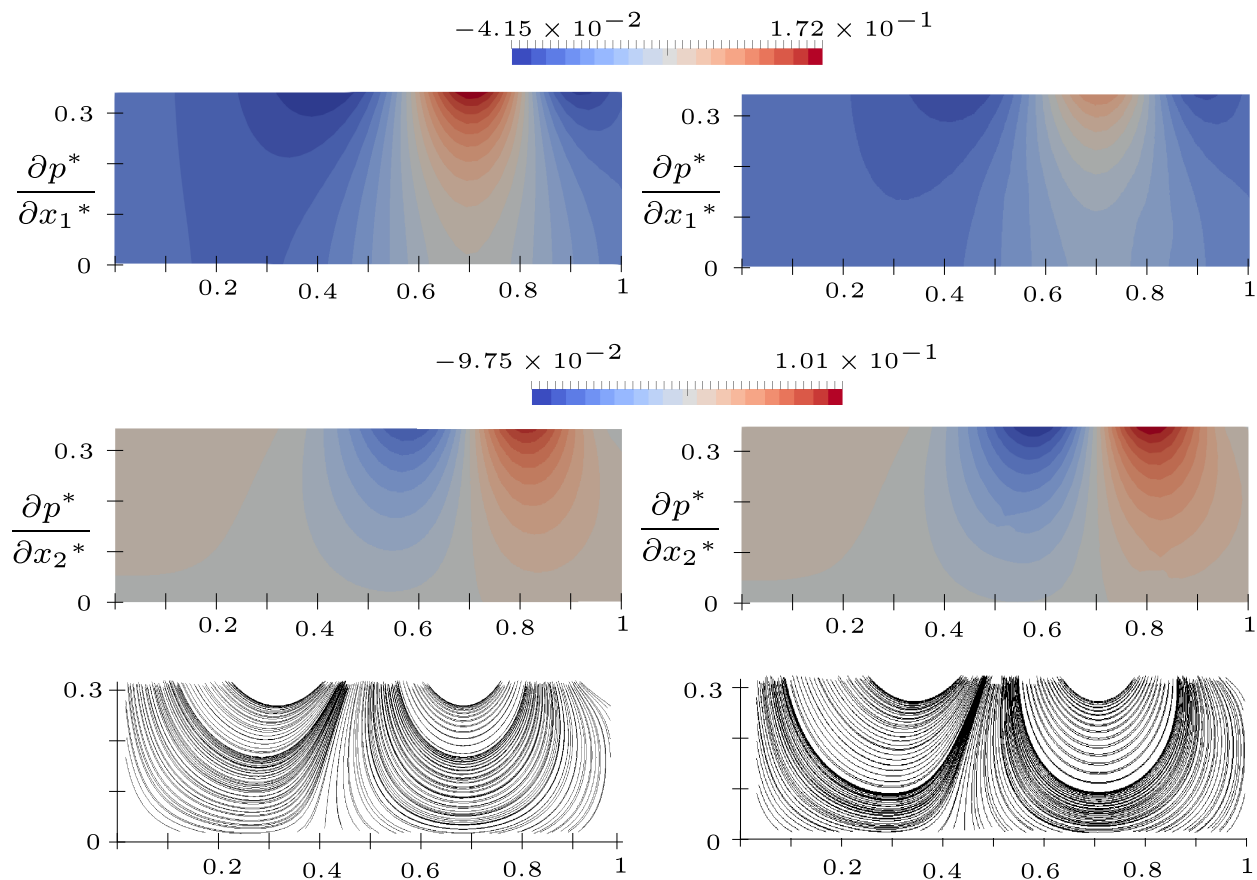
FIG. 5: Left: VANS approach. Right: Homogenized DNS approach. The figures show, from top to bottom, the two components of the pressure gradient and the streamlines inside the porous domain Ω_p for $Re = 1000$.

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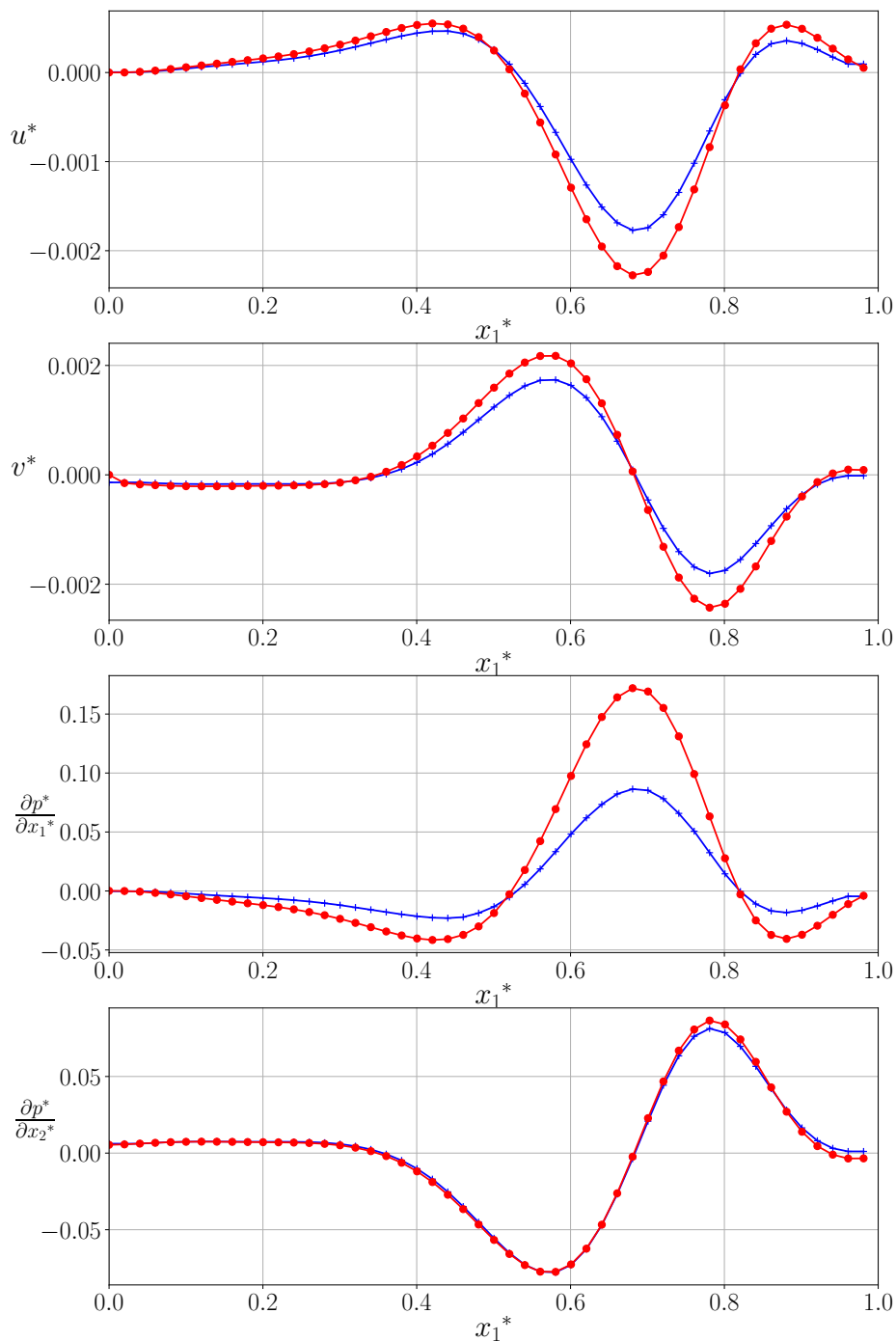
FIG. 6: View of the macroscopic profile of u^*, v^*, $\frac{\partial p^*}{\partial x_1^*}$ and $\frac{\partial p^*}{\partial x_2^*}$, for $x_2^* = 0.33$ (interface position) for the VANS (red lines with circles) and the DNS approaches (blue lines with crosses) at $Re = 1000$.

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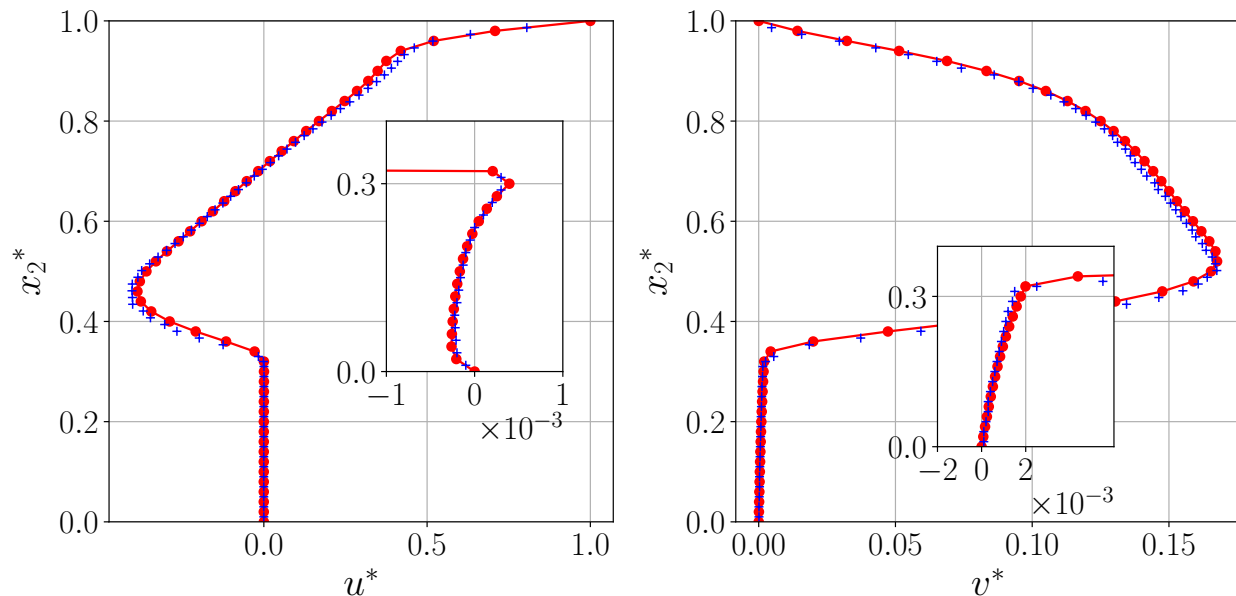
FIG. 7: View of the macroscopic profile of u^* (left frame) and v^* (right frames) for $x_1^* = 0.5$ (middle of the cavity) for the VANS (red line with circles) and the DNS approaches (blue line with crosses) at $Re = 1000$.

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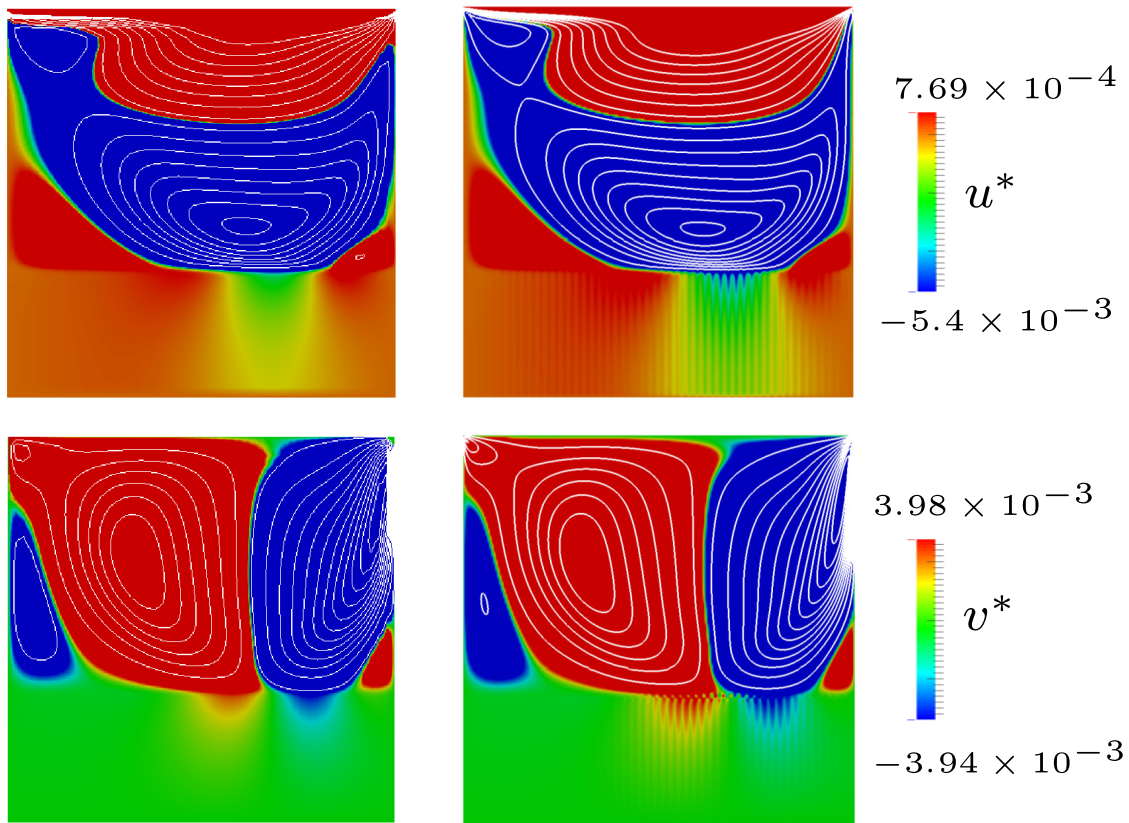
FIG. 8: Left: VANS approach. Right: Homogenized DNS approach. The figures show the horizontal velocity component in the whole domain. In the bottom figures the range of values plotted has been reduced to highlight the flow structure within the fibers in the DNS case for $Re = 1000$.

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